

# Numerical Study Of The Effect Of Hydrogen Addition On The Laminar Flame Speed And Premixed Flame Structure Of Biogas

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**Abstract-** In this work, the laminar flame speed and flame structure of biogas/H<sub>2</sub> fuel mixtures were studied numerically from pure biogas to biogas with an addition of 15% H<sub>2</sub> in volume by using the CHEMKIN software with the GRIMECH 2.11 kinetic mechanism. The effect of hydrogen addition to biogas on laminar flame speed and flame structure has been studied as well as the variation of the aeration rate from stoichiometric conditions to lean conditions. The trends in laminar flame speed results obtained are explained by means of numerical results on temperature profile and heat release rate. CO, CO<sub>2</sub> and NO profiles are also observed for the different mixtures studied. Hydrogen addition in biogas flames shows an important effect, especially in zones near stoichiometric flames, decreasing its effects in lean mixtures combustion.

**Keywords** Biogas-hydrogen, laminar flame speed, flame structure, numerical study.

## 1. Introduction

The necessary use of combustion technologies to reduce the dependence on fossil fuels [1] and additionally, the emission of greenhouse gases to meet the goals of climate change mitigation [2,3], have generated a continuous growth in the study [4] of the possible applications of alternative fuels such as biogas generated by anaerobic decomposition of organic substances, synthesis gas produced in the gasification of coal or biomass, liquid biofuels as fuel alcohol obtained from different crops such as corn or sugar cane and biodiesel obtained from vegetable oils.

Biogas generated by the anaerobic decomposition of organic substances is a great source of energy, especially in regions or countries where economic growth causes an increasing in the generation of municipal solid waste or organic waste product of industrial or agricultural activities where its decomposition could generate this alternative fuel [3,5-7]. This biogas, composed mainly of methane (CH<sub>4</sub>), carbon dioxide (CO<sub>2</sub>) and other small amounts of oxygen, nitrogen, volatile compounds and even hydrogen sulphide, is generally cleaned of some of these minor compounds [8] to reduce their harmful effect on combustion systems.

The clean biogas (CH<sub>4</sub> and CO<sub>2</sub>) is a fuel whose combustion properties such as calorific value, flame

temperature and deflagration velocity are poor compared to conventional gaseous fuels such as natural gas or LPG [9-12]. This produces that the use of the biogas in combustion systems requires a study to that avoid the problems of flame instability associated to the lower flame speed and the change in the limits of flammability [13-16]. However, in [17], it is concluded that the use of biogas in burners for natural gas does not require significant modifications in the burners based on the profile of flame temperatures and pollutant emissions, but not on flame stability parameters. One of the ways to improve these combustion properties in to convert biogas to biomethane using different treatments that reduce the CO<sub>2</sub> content and its effects [18,19] as well as other minor compounds such as H<sub>2</sub>S [8,20,21]. However, this treatment process is expensive in terms of equipment and absorbing substances such as amines. The improvement of the combustion properties of the biogas can be achieved by mixing it with another combustible gas whose combustion properties, mainly the flame speed, is greater so that the resulting mixture has combustion properties that can be compared with those of the gas Natural or LPG, reducing the problems of biogas interchangeability with these fuels [9, 22]. Hydrogen is the combustible gas that has the greatest value of flame speed at standard conditions, in addition to a higher calorific value, a higher flammability range and a higher flame temperature, and therefore, its addition to the biogas will result in an improvement of the combustion properties of this last

one. Different studies have concluded that mixing the biogas with other fuels such as H<sub>2</sub>, LPG or natural gas increases the flame speed of the resulting mixture and therefore the range of flame stability [23-27]. Hydrogen has been selected as the biogas additive to improve its combustion properties since it is a renewable fuel, with a zero greenhouse potential and which could additionally be obtained from fossil fuels through reforming processes [28] or even from the same biogas [29,30].

By means of the realization of a numerical study, it has been studied the effect of hydrogen addition on the flame structure of biogas [31,32], biogas/H<sub>2</sub> mixtures in diffusion flames [33], methane with CO<sub>2</sub> dilution [34] and syngas [35]. In this work, it is tried to determine the effect of the addition of different proportions of H<sub>2</sub> to a simulated biogas in the flame speed and flame structure of premixed flames. The results are intended to guide the H<sub>2</sub> produced from reforming other fossil fuels as an alternative to improve the combustion properties of biogas, especially in atmospheric premix burners.

## 2. Methodology

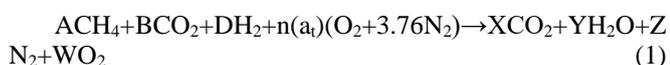
Different numerical simulations of biogas combustion reactions were performed in the CHEMKIN Software. Simulations of the combustion reactions of different mixtures have been performed for different aeration factors, starting with a stoichiometric mixture and increasing these aeration factors as shown in Table 1.

**Table 1.** Composition of biogas and biogas/H<sub>2</sub> mixtures simulated

Mixture	Composition	Aeration factor n				
		1	1.1	1.2	1.3	1.4
Pure biogas	0.6CH <sub>4</sub> + 0.4CO <sub>2</sub>	1	1.1	1.2	1.3	1.4
Biogas + 5% H <sub>2</sub>	0.57CH <sub>4</sub> + 0.38CO <sub>2</sub> + 0.05H <sub>2</sub>	1	1.1	1.2	1.3	1.4
Biogas + 15% H <sub>2</sub>	0.51CH <sub>4</sub> + 0.34CO <sub>2</sub> + 0.15H <sub>2</sub>	1	1.1	1.2	1.3	1.4

The composition for the simulated biogas was selected as shown in Table 1 for pure biogas. This is a mean composition for a biogas typically generated in landfills or wastewater treatment plants or bio digesters of organics waste, taking into account the difficulty of finding typical biogas generation data in the literature [36]. Similar mean compositions are presents in [33-35,37,38].

The aeration factor n for combustion is introduced into the stoichiometric equation of each reaction as given below:



Where n is the aeration factor and a<sub>i</sub> is the theoretical air coefficient of the combustion reaction determined by the elementary reaction balances. The values of aeration factor was selected only for fuel lean mixtures (n > 1) to support a subsequent experimental stage of the project using an atmospheric premix burner.

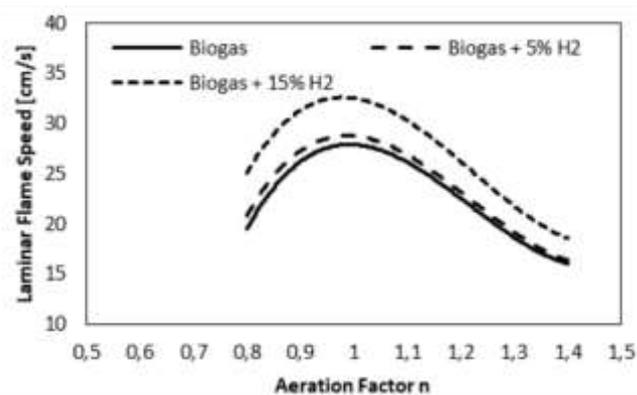
The CHEMKIN tool has been used to determine the laminar flame speed of the specified combustible gas mixtures. The chemical kinetics and transport equations for gas phase are solved following the free-propagation flame model to obtain the chemical species concentration profiles, the heat release rate and the temperature profile developed for adiabatic flame starting from the molar compositions of each of the selected mixtures described above and with initial values of the pressure at which the flame is developed and an approximate temperature profile. For these simulations, site conditions of pressure and temperature of 0.91 atm and 298 K were established and the chemical kinetics mechanisms Grimech 2.11 was used, mechanism that have been validated for the simulation of biogas flames [39-41].

## 3. Results and Discussion

The results of the simulations obtained in the estimation of the laminar deflagration velocity of the studied mixtures and its temperature profile, heat release rate and species profiles are presented and discussed.

### 3.1 Laminar Flame Speed

Numerical results of laminar flame speed obtained according with the methodology presented, for the mixtures before mentioned are shown in Figure 1. This laminar flame speed has been obtained for the different aeration factors presented in Table 1.



**Fig. 1.** Laminar flame speed of pure Biogas and Biogas/H<sub>2</sub> mixtures with variation of aeration factor.

The values obtained in this work for pure biogas (continuous line); shown in Figure 1, agree with reported values for biogas flames [22, 24] between 27 and 28 cm/s respectively for stoichiometric flames and similar pressure and temperature conditions. The maximum value of the laminar flame speed for the biogas/H<sub>2</sub> mixtures is reached, with values ranging from 27.4 m/s for pure biogas and 28.47 and 32.17 m/s for biogas with 5% H<sub>2</sub> and biogas with 15% H<sub>2</sub>

respectively. For lean mixtures ( $n=1.4$ ), the effect of hydrogen addition on laminar flame speed decreases, from values of 15.8 cm/s for pure biogas to 18.41 cm/s for biogas with 15%  $H_2$ . The effect of 5% of hydrogen addition in the laminar flame speed of biogas represents a small change from the pure biogas; therefore, according to results obtained, a significant improvement on laminar flame speed of biogas requires a hydrogen addition near 15% or more in volume.

### 3.2 Flame Structure

Observing the flame structure obtained in the different simulations, we can relate the observed increase in the flame speed with the effect of hydrogen on the kinetics of the reaction. Figures 2-4 show the temperature profiles for stoichiometric mixtures ( $n = 1$ ) and lean mixtures ( $n = 1.2$  and  $n = 1.4$ ).

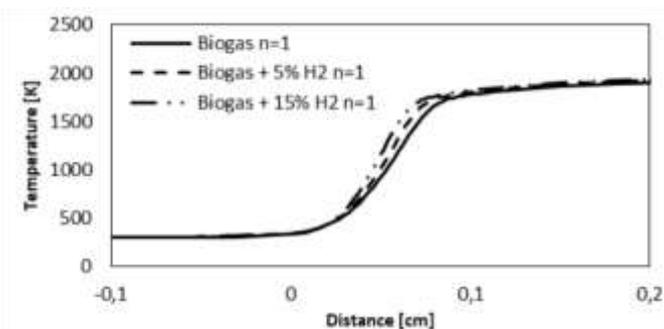


Fig. 2. Temperature profile of the reaction zone for biogas/ $H_2$  mixtures with  $n = 1$

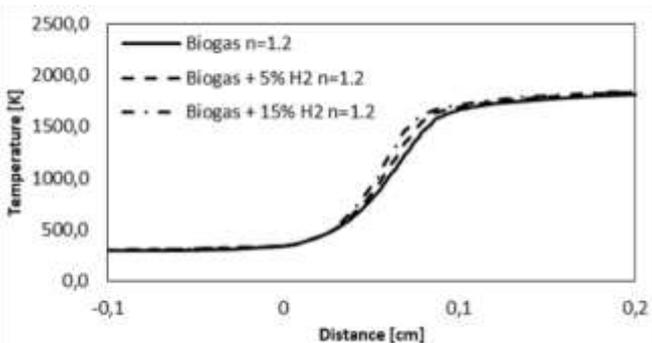


Fig. 3. Temperature profile of the reaction zone for biogas/ $H_2$  mixtures with  $n = 1.2$

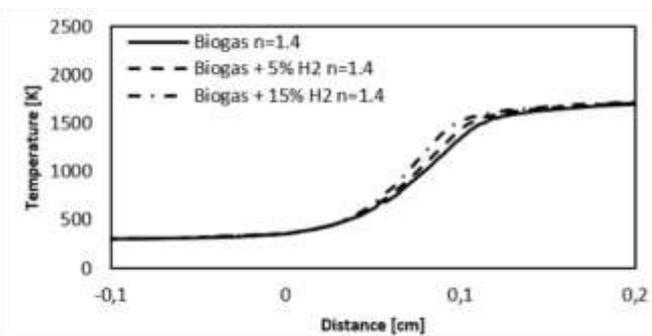


Fig. 4. Temperature profile of the reaction zone for biogas/ $H_2$  mixtures with  $n = 1.4$

As can be seen, the hydrogen addition to the biogas generates an acceleration of the combustion reaction. This being reflected in higher temperature gradients in the reaction zone and resulting in higher rates of heat release, which ultimately cause less thickness of the reaction zone, which is indicative of the increase in the flame speed [42,43]. The temperature profile for pure biogas of this work agree with results shown in [34]. In Figs. 5-7, it can be observed the effect of hydrogen addition in heat release rate of combustion reactions.

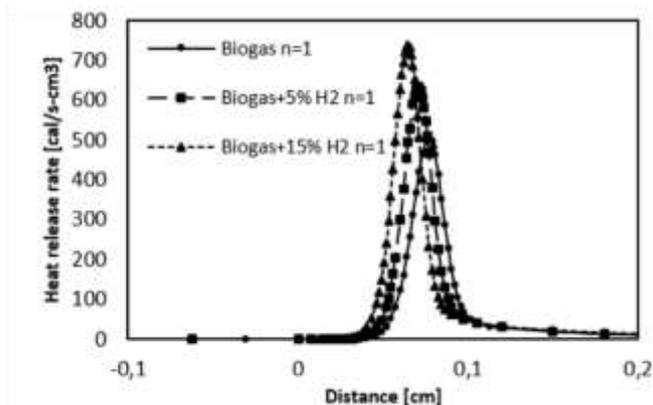


Fig. 5. Heat release rate for biogas/ $H_2$  mixtures with  $n = 1$

For stoichiometric mixtures, pure biogas presents a value of this maximum heat release rate of 508 cal/s-cm<sup>3</sup>. Addition of 5% of hydrogen causes a maximum rate of heat release of 634 cal/s-cm<sup>3</sup> and an addition of 15% of hydrogen generates a maximum rate of heat release of 738 cal/s-cm<sup>3</sup>. This increase in this parameter is reflected in the flame speed.

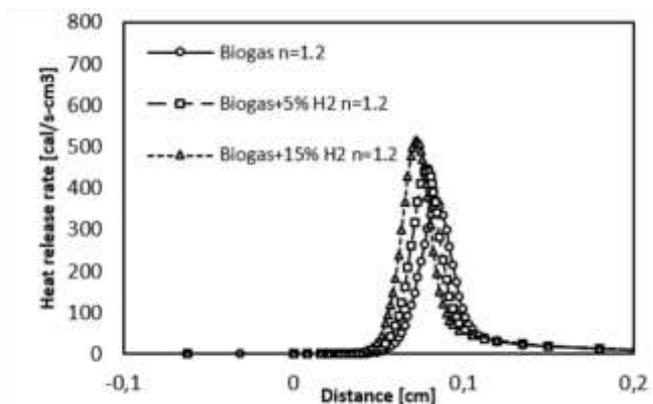


Fig. 6. Heat release rate for biogas/ $H_2$  mixtures with  $n = 1.2$

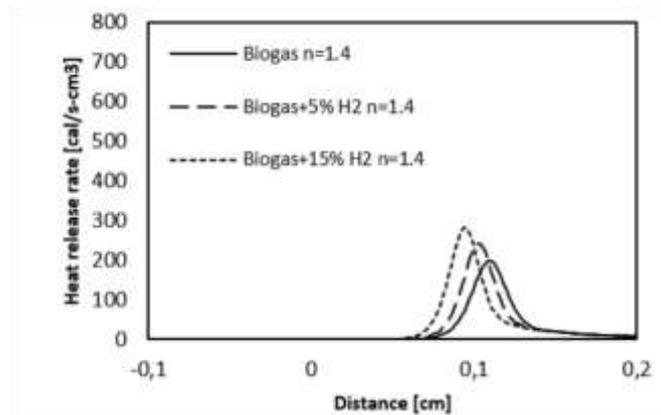


Fig. 7. Heat release rate for biogas/H<sub>2</sub> mixtures with n = 1.4

For the biogas/H<sub>2</sub> mixtures with aeration factor n = 1.2, it can be seen that the maximum value of the heat release rate for pure biogas is 366 cal/s-cm<sup>3</sup>, increasing to 446 cal/s-cm<sup>3</sup> for mixing with 5% H<sub>2</sub> and 516 cal/s-cm<sup>3</sup> for mixing with 15% H<sub>2</sub>. In this case, the increase in the rate of heat release presents a less noticeable increase than in the stoichiometric flame, as it is also observed in the flame speed. Finally, for lean flames (n = 1.4), the values of the heat release rate have values from 199 cal/s-cm<sup>3</sup> for pure biogas and 243 cal/s-cm<sup>3</sup> and 283 cal/s-cm<sup>3</sup> for Mixtures with 5% H<sub>2</sub> and 15% H<sub>2</sub> respectively. Reported value for heat release rate in [10], for a stoichiometric flame of biogas with 25% CO<sub>2</sub> is near to 800 cal/s-cm<sup>3</sup> and for an aeration factor of 1.25, is reported a heat release rate near of 570 cal/s-cm<sup>3</sup>, indicating a similar trend in this results. For a similar biogas used in this work, the reported value of heat release rate in [18] agrees with the result obtained in this work, approximately 500 cal/s-cm<sup>3</sup>.

As noted, the increase in the rate of heat release in these lean mixtures is less noticeable in absolute terms but similar in percentages (45% for stoichiometric mixture, 40% and 42% for lean mixtures). Furthermore, a little displacement in the coordinate where the reaction is developed is observed as hydrogen percentage increases, indicating the possibility of flame instability.

The relation between temperature profile and heat release rate is shown in Figure 8 and Figure 9 for stoichiometric mixtures and lean mixtures respectively.

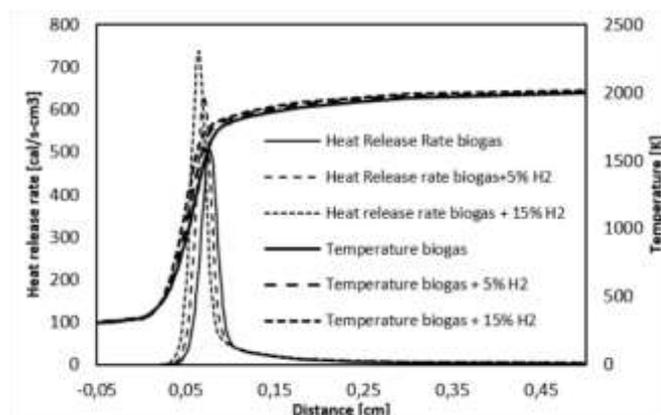


Fig. 8. Temperature profiles and heat release rate for biogas/H<sub>2</sub> mixtures with n = 1

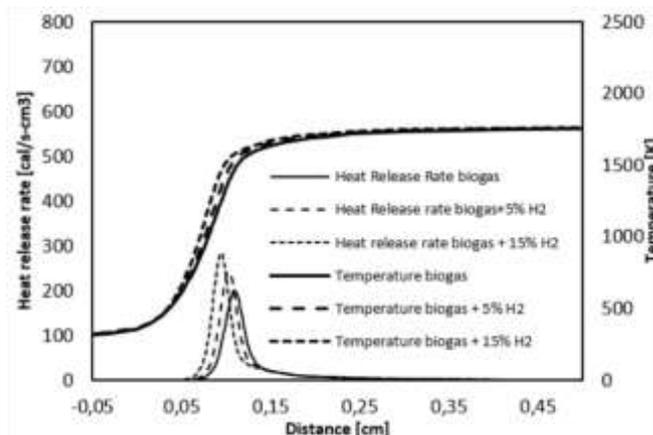


Fig. 9. Temperature profiles and heat release rate for biogas/H<sub>2</sub> mixtures with n = 1.4

As we can see, the hydrogen addition has a more important effect in stoichiometric mixtures but only this effect is noticeable in the heat release rate. The temperature profile remains almost unaltered for biogas/H<sub>2</sub> mixtures in each simulated aeration factor.

Regarding chemical species, hydrogen addition has a significant effect on the decreasing of carbon dioxide emission. In Figs. 10 and 11 it can be observed the effect in carbon dioxide emission of hydrogen addition to biogas for stoichiometric and lean mixtures respectively.

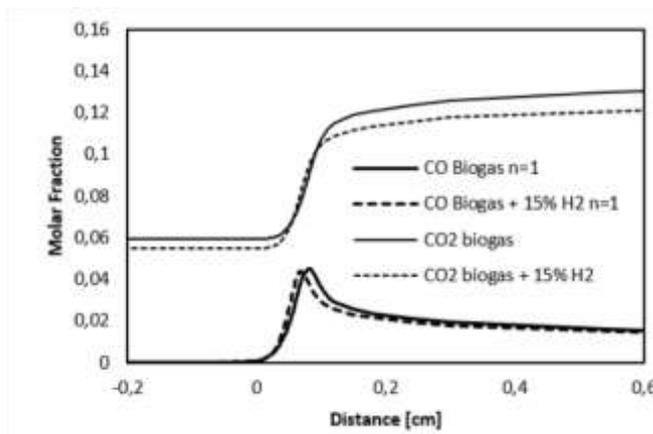
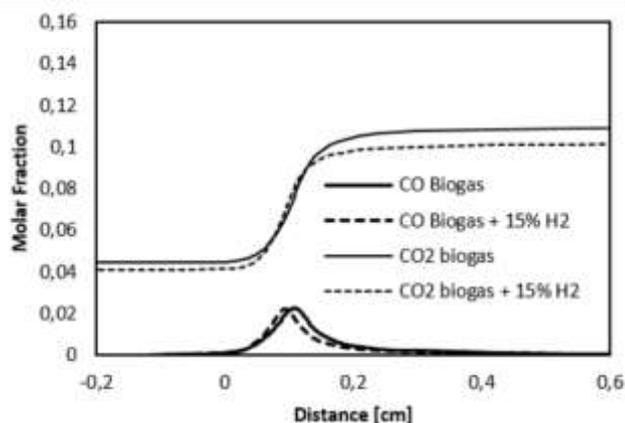
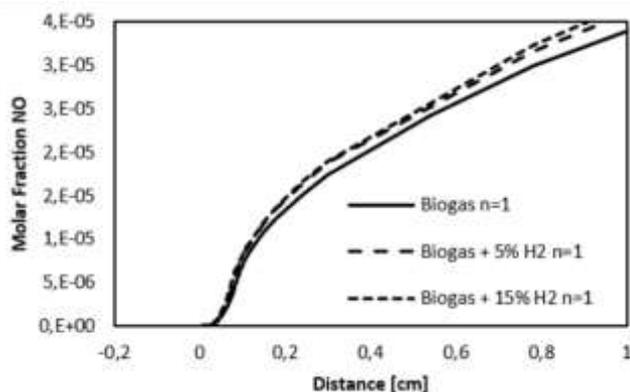


Fig. 10. CO and CO<sub>2</sub> profile for biogas/H<sub>2</sub> stoichiometric mixtures n=1



**Fig. 11.** CO and CO<sub>2</sub> profile for biogas/H<sub>2</sub> lean mixtures n=1.4

Hydrogen addition has not a significant effect in carbon monoxide emission under the adiabatic combustion supposition used. Similar results for CO and CO<sub>2</sub> concentration is presented in [10] for stoichiometric combustion of a 50% CH<sub>4</sub>/CO<sub>2</sub> biogas. Finally, the effect in NO formation is shown in Figure 12. Only results for stoichiometric mixtures are shown due to for lean mixtures, NO formation is restricted by lower temperatures obtained. These conditions prevent the activation of the NO<sub>x</sub> formation zeldovich thermal mechanism, this being the main NO<sub>x</sub> formation mechanism in the combustion of gases upon the prompt mechanism and the formation mechanism due to the N<sub>2</sub> of the fuel due to the absence of N<sub>2</sub> in the biogas simulated in this work [44-47].



**Fig. 12.** NO profile for biogas/H<sub>2</sub> stoichiometric mixtures n=1

As can be seen, hydrogen addition to biogas may generate an increase in NO formation; however, this increase is only appreciable for stoichiometric conditions. It may be due to the higher temperature gradients and heat release rates obtained with the hydrogen addition. These conditions activate the Zeldovich thermal mechanism of NO formation how was explained before.

#### 4. Conclusions

In this work, the laminar flame speed and flame structure of biogas and biogas/H<sub>2</sub> mixtures have been studied numerically under normal conditions. The results obtained shown the influence of hydrogen addition and the aeration rate on the laminar flame speed and flame structure of the mixtures studied.

The main results allow us to conclude that the laminar flame speed of the biogas under normal conditions and stoichiometric conditions reaches a value of 27.4 m/s. The addition of hydrogen allows increasing this velocity to values of 32.17 m/s with a 15% addition of H<sub>2</sub>, implying an increase of up to 16% of this parameter. However, under lean conditions, the increase in laminar flame speed between pure biogas and the addition of 15% H<sub>2</sub> only reaches approximately 5% according to results presented. The increase in the laminar flame speed can be divided into two zones, one close to stoichiometric mixtures where a significant increase is observed and another one of lean mixtures where this increase is less noticeable. This indicates that the addition of hydrogen to biogas can facilitate the use of biogas/H<sub>2</sub> mixtures in replacement of other gases such as natural gas or LPG under conditions close to stoichiometric combustion but for conditions of high aeration of other gases, where their laminar flame speeds may be similar to those obtained for biogas/H<sub>2</sub> mixtures.

The addition of H<sub>2</sub> to the biogas generates an increase in the kinetics of the reaction. This is reflected in the higher temperature gradients in the reaction zone of mixtures with higher H<sub>2</sub> content and higher rates of release of heat in the reaction zone. It can be seen a different behavior to the laminar flame speed (where there is a relative increase), since in mixtures close to the stoichiometric one has an increase in this rate of up to 45% according to the results obtained and of 40% and 42% in lean mixtures.

Finally, the hydrogen addition to biogas has an effect of decreasing of carbon dioxide concentration in the flue gas, which can be seen as a beneficial effect in the reduction of emissions of greenhouse gases, however, the hydrogen addition has not and appreciable effect on carbon monoxide concentration for stoichiometric and lean conditions. The higher temperature gradients and heat release rate obtained with hydrogen addition cause a higher NO concentration in biogas flames and a displacement of the reaction zone toward reactants, which can create problems of flame instability due to the higher laminar flame speed of hydrogen.

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## References

- [1] M. R. Al Mamun and S. Torii, "Anaerobic co-digestion of cafeteria, vegetable and fruit wastes for biogas production," in *2014 International Conference on Renewable Energy Research and Application (ICRERA)*, 2014.
- [2] G. Mundaca, "How much can CO<sub>2</sub> emissions be reduced if fossil fuel subsidies are removed?" *Energy Econ*, vol. 64, pp. 91-104, 2017.
- [3] (MNRE), Ministry of New and Renewable Energy and MNRE, "Biogas Power (Off-grid) Programme," vol. 2016, 2016.
- [4] M. A. Sanz-Bobi, F. De Cuadra and C. Batlle, "A review of key points of an industrial biogas plant. A European perspective" in *International Conference on Renewable Energy Research and Applications (ICRERA)*, 2012.
- [5] W. Ortiz, J. Terrapon-Pfaff and C. Dienst, "Understanding the diffusion of domestic biogas technologies. Systematic conceptualization of existing evidence from developing and emerging countries," *Renewable and Sustainable Energy Reviews*, vol. 74, pp. 1287-1299, 2017.
- [6] I. Perez, M. Garf, E. Cadena and I. Ferrer, "Technical, economic and environmental assessment of household biogas digesters for rural communities," *Renewable Energy*, vol. 62, pp. 313-318, 2014.
- [7] K.C. Surendra, D. Takara, A.G. Hashimoto and S.K. Khanal, "Biogas as a sustainable energy source for developing countries: Opportunities and challenges," *Renewable and Sustainable Energy Reviews*, vol. 31, pp. 846-859, 2014.
- [8] R. Kadam and N.L. Panwar, "Recent advancement in biogas enrichment and its applications," *Renewable and Sustainable Energy Reviews*, vol. 73, pp. 892-903, 2017.
- [9] C. Diaz-Gonzalez, A. Arrieta and J. Suarez, "Comparison of combustion properties of simulated biogas and methane," *Ci&f-Ciencia, Tecnología Y Futuro*, vol. 3, pp. 225-236, 2009.
- [10] Z.L. Wei, C.W. Leung, C.S. Cheung and Z.H. Huang, "Effects of equivalence ratio, H<sub>2</sub> and CO<sub>2</sub> addition on the heat release characteristics of premixed laminar biogas-hydrogen flame," *Int J Hydrogen Energy*, vol. 41, pp. 6567-6580, 2016.
- [11] C. Lee, C. Oh, I. Jung and J. Park, "A study on the determination of burning velocities of LFG and LFG-mixed fuels," *Fuel*, vol. 81, pp. 1679-1686, 2002.
- [12] L. Pizzuti, C.A. Martins and P.T. Lacava, "Laminar burning velocity and flammability limits in biogas: A literature review," *Renewable and Sustainable Energy Reviews*, vol. 62, pp. 856-865, 2016.
- [13] C. Lee and C. Hwang, "An experimental study on the flame stability of LFG and LFG-mixed fuels," *Fuel*, vol. 86, pp. 649-655, 2007.
- [14] C.A. Diaz Gonzalez, A. Amell Arrieta and L.F. Cardona, "Estudio experimental de la estabilidad de llama de biogás en un sistema de premezcla," *Energética*, 2008.
- [15] L. Pizzuti, F.A. Torres, R.W. Ferreira, L.R. Santos, P.T. Lacava and C.A. Martins, "Laminar burning velocity and flammability limits in Biogas: A state of the art" in *International Conference on Heat Transfer, Fluid Mechanics and Thermodynamics*, 2014.
- [16] W. Anggono, "Behaviour of Biogas Containing Nitrogen on Flammability Limits and Laminar Burning Velocities," *Int. J. of Renewable Energy Research*, vol. 7, (1), pp. 304-310, 2017.
- [17] M. Ilbas, M. Sahin and S. Karyeyen, "Combustion Behaviours of Different Biogases in an Existing Conventional Natural Gas Burner: An Experimental Study," *Int. J. of Renewable Energy Research (IJRER)*, vol. 6, (3), pp. 1178-1188, 2016.
- [18] H. Nonaka and F.M. Pereira, "Experimental and numerical study of CO<sub>2</sub> content effects on the laminar burning velocity of biogas," *Fuel*, vol. 182, pp. 382-390, 2016.
- [19] N. Hamidi, "Carbon Dioxide Effects on the Flammability Characteristics of Biogas," *Applied Mechanics and Materials*, pp. 129-133, 2014.
- [20] K. Biernat, W. Gis and I. Samson-Bręk, "Review of technology for cleaning biogas to natural gas quality," *Combustion Engines*, vol. 148, pp. 33-39, 2012.
- [21] M.J. Khalil, K. Sharma and R. Gupta, "Strategic Technologies for biogas purification," in *International journal of Engineering and Technical Research* ISSN: 2321-0869, Special Issue. National Conference on Synergetic trends in Engineering and Technology (STET-2014), 2014.
- [22] W. Qin, F.N. Egolfopoulos and T.T. Tsotsis, "Fundamental and environmental aspects of landfill gas utilization for power generation," *Chem. Eng. J.*, vol. 82, pp. 157-172, 2001.
- [23] S.E. Hosseini and M.A. Wahid, "Development of biogas combustion in combined heat and power generation," *Renewable & Sustainable Energy Reviews*, vol. 40, pp. 868-875, December 1. 2014.
- [24] C.A. Cardona and A.A. Amell, "Laminar burning velocity and interchangeability analysis of biogas/C<sub>3</sub>H<sub>8</sub>/H<sub>2</sub> with normal and oxygen-enriched air," *Int. J Hydrogen Energy*, vol. 38, pp. 7994-8001, 2013.
- [25] H.S. Zhen, C.W. Leung, C.S. Cheung and Z.H. Huang, "Characterization of biogas-hydrogen premixed flames using Bunsen burner," *Int. J Hydrogen Energy*, vol. 39, pp. 13292-13299, 2014.
- [26] F. Coppens, J. De Ruyck and A.A. Konnov, "Effects of hydrogen enrichment on adiabatic burning velocity and NO formation in methane air flames," *Exp. Therm. Fluid Sci.*, vol. 31, pp. 437-444, 2007.
- [27] V. Di Sarli and A. Di Benedetto, "Laminar burning velocity of hydrogen-methane/air premixed flames," *Int. J. Hydrogen Energy*, vol. 32, pp. 637-646, 2007.
- [28] L. Pacheco, D. Della-Valle, O. Le Corre, C. Habchi, T. Lemenand and H. Peerhossaini, "Modeling Open-Flow Steam Reforming of Methanol over Cu/ZnO/Al<sub>2</sub>O<sub>3</sub> Catalyst in an Axisymmetric Reactor." *Journal of Applied Fluid Mechanics*, vol. 8, pp. 33-42, 2015.
- [29] G. Nahar, D. Mote and V. Dupont, "Hydrogen production from reforming of biogas: Review of technological advances and an Indian perspective," *Renewable and Sustainable Energy Reviews*, vol. 76, pp. 1032-1052, 2017.
- [30] S. Kaya, B. Ozturk and H. Aykac, "Hydrogen production from renewable source: Biogas" in *International*

- Conference on Renewable Energy Research and Applications (ICRERA)*, 2013.
- [31] C.A. Hoerlle, L. Zimmer and F.M. Pereira, "Numerical study of CO<sub>2</sub> effects on laminar non-premixed biogas flames employing a global kinetic mechanism and the Flamelet-Generated Manifold technique," *Fuel*, vol. 203, pp. 671-685, 2017.
- [32] A. Greco, D. Mira and X. Jiang, "Effects of Fuel Composition on Biogas Combustion in Premixed Laminar Flames," *Energy Procedia*, vol. 105, pp. 1058-1062, 2017.
- [33] A. Mameri and F. Tabet, "Numerical investigation of counter-flow diffusion flame of biogas-hydrogen blends: effects of biogas composition, hydrogen enrichment and scalar dissipation rate on flame structure and emissions," *Int J Hydrogen Energy*, vol. 41, pp. 2011-2022, 2016.
- [34] M.A.M. Patio, D. Alviso and R.G. dos Santos, "Numerical Study of Laminar Premixed Methane/Air Flames With Carbon Dioxide Dilution," in *16th Brazilian Congress of Thermal Sciences and Engineering*, pp. 1-6, 2016.
- [35] S. Yousefian, A. Ghafourian and M. Darbandi, "Numerical Study of Syngas Premixed Flame Structure and Extinction," *Proc. Combust. Inst.*, 2011.
- [36] V. Yilmaz, "A straightforward method: Biochemical methane potential assay," in *International Conference on Renewable Energy Research and Applications (ICRERA)*, 2015.
- [37] E. U. Khan and A. R. Martin, "Hybrid renewable energy with membrane distillation polygeneration for rural households in Bangladesh: Pani Para village case study," in *International Conference on Renewable Energy Research and Application (ICRERA)*, 2014.
- [38] P. Sefeedpari, S. Rafiee and A. Akram, "Providing electricity requirements by biogas production and its environmental benefit in sample dairy farms of Iran," *Int. J. of Renewable Energy Research (IJRER)*, vol. 2, (3), pp. 384-387, 2012.
- [39] R. Bardolf and F. Winter, "Comparison of chemical kinetic mechanisms for combustion simulation of treated biogas," *The Holistic Approach to Environment*, vol. 4, pp. 65-69, 2014.
- [40] S. Jahangirian and A. Engeda, "Biogas combustion and chemical kinetics for gas turbine applications," in *Proceedings of the ASME International Mechanical Engineering Conference and Exposition*, 2008.
- [41] M. Kuznia, W. Jerzak, P. Lyko and J. Sikora, "Analysis of the combustion products of biogas produced from organic municipal waste," *Journal of Power Technologies*, vol. 95, pp. 158, 2015.
- [42] R.J. Blint, "The relationship of the laminar flame width to flame speed," *Combustion Sci. Technol.*, vol. 49, pp. 79-92, 1986.
- [43] B. Lewis and G. Von Elbe, *Combustion, flames and explosions of gases*, Elsevier, 2012.
- [44] Turns S. *An introduction to combustion*. 1996.
- [45] Glassman, R. A. Yetter and N. G. Glumac, *Combustion*. 2014.
- [46] D. Bohn and J. Lepers, "Effects of biogas combustion on the operation characteristics and pollutant emissions of a micro gas turbine," in *ASME Turbo Expo 2003, Collocated with the 2003 International Joint Power Generation Conference*, 2003.
- [47] A. Frassoldati, T. Faravelli and E. Ranzi, "A wide range modeling study of NO<sub>x</sub> formation and nitrogen chemistry in hydrogen combustion," *Int J Hydrogen Energy*, vol. 31, (15), pp. 2310-2328, 2006.